

AMENDMENTS TO THE CLAIMS

This Listing of Claims will replace all prior versions and listings of claims in this application.

Listing of Claims:

1. (Currently Amended) A process for obtaining oligomers of polytetrahydrofuran or of tetrahydrofuran copolymers from a methanolic crude product which contains polytetrahydrofuran or tetrahydrofuran copolymers and is obtained in the transesterification of the mono- and/or diesters of polytetrahydrofuran or tetrahydrofuran copolymers with methanol, which comprises:
 - a) removing the majority of the methanol from the crude product in a first distillation stage;
 - b) separating the resulting bottom product by distillation into a top fraction comprising the oligomers of polytetrahydrofuran or of tetrahydrofuran copolymers, and polytetrahydrofuran or tetrahydrofuran copolymer; and
 - c) condensing the oligomers of polytetrahydrofuran or of tetrahydrofuran copolymers out of the top fraction from stage b).
2. (Original) A process as claimed in claim 1, wherein the methanol removed in stage a) is recycled into the transesterification.
3. (Previously Presented) A process as claimed in claim 1, wherein distillation is effected in stage a) at from 20 to 500 mbar gauge and a temperature of from 50 to 250°C.
4. (Previously Presented) A process as claimed in claim 1, wherein distillation is effected in stage b) at an absolute pressure of from 1 to 300 mbar and at from 50 to 250°C.
5. (Previously Presented) A process as claimed in claim 1, wherein condensation is effected in stage c) at a temperature of from 5 to 40°C.

6. (Currently Amended) A process as claimed in claim 1, wherein the crude product obtained is freed before stage a) of sodium ions stemming from a the transesterification catalyst by treatment with an ion exchanger.
7. (Previously Presented) A process as claimed in claim 2, wherein distillation is effected in stage a) at from 20 to 500 mbar gauge and a temperature of from 50 to 250°C.
8. (Previously Presented) A process as claimed in claim 2, wherein distillation is effected in stage b) at an absolute pressure of from 1 to 300 mbar and at from 50 to 250°C.
9. (Previously Presented) A process as claimed in claim 3, wherein distillation is effected in stage b) at an absolute pressure of from 1 to 300 mbar and at from 50 to 250°C.
10. (Previously Presented) A process as claimed in claim 2, wherein condensation is effected in stage c) at a temperature of from 5 to 40°C.
11. (Previously Presented) A process as claimed in claim 3, wherein condensation is effected in stage c) at a temperature of from 5 to 40°C.
12. (Previously Presented) A process as claimed in claim 4, wherein condensation is effected in stage c) at a temperature of from 5 to 40°C.
13. (Currently Amended) A process as claimed in claim 2, wherein the crude product obtained is freed before stage a) of sodium ions stemming from a the transesterification catalyst by treatment with an ion exchanger.
14. (Currently Amended) A process as claimed in claim 3, wherein the crude product obtained is freed before stage a) of sodium ions stemming from a the transesterification catalyst by treatment with an ion exchanger.
15. (Currently Amended) A process as claimed in claim 4, wherein the crude product obtained is freed before stage a) of sodium ions stemming from a the transesterification catalyst by treatment with an ion exchanger.

16. (Currently Amended) A process as claimed in claim 5, wherein the crude product obtained is freed before stage a) of sodium ions stemming from a the transesterification catalyst by treatment with an ion exchanger.